Microbial fuel cells a state-of-the-art technology for wastewater treatment and bioelectricity generation

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16 Abstract

17 Wastewater treatment and electricity generation have been the major concerns for the last few 18 years. The scarcity of fossil fuels has led to the development of unconventional energy resources 19 that are pollution-free. Microbial fuel cell (MFC) is an environmental and eco-friendly technology 20 that harvests energy through the oxidation of organic substrates and transform into the electric 21 current with the aid of microorganisms as catalysts. This review presents power output and colour 22 removal values by designing various configurations of MFCs and highlights the importance of 23 materials for the fabrication of anode and cathode electrodes playing vital roles in the formation 24 of biofilm and redox reactions taking place in both chambers. The electron transfer mechanism 25 from microbes towards the electrode surface and the generation of electric current are also highlighted. The effect of various parameters affecting the cell performance such as type and 26 27 amount of substrate, pH and temperature maintained within the chambers have also been

discussed. Although this technology presents many advantages, it still needs to be used incombination with other processes to enhance power output.

30 Keywords: Environmental sustainability; Wastewater treatment; Microbial fuel cell;
 31 Configurations; Electron transfer mechanism; Electrode fabrication and Bioenergy.

32 **1 Introduction**

33 Nonrenewable energy resources have been excessively utilized to meet energy demand [1]. The 34 scarcity of fossil fuels and their influence on climate change has put forward the requirement to 35 search for some alternative energy resources. Many disadvantages associated with conventional 36 treatment methods such as the generation of huge quantities of sludge that need further treatment 37 for their disposal lead to several financial issues [2, 3]. Therefore, there is an intense need of using 38 such energy sources that lead to a pollution-free environment [4, 5]. Because of the presence of a 39 number of impurities and toxic components, wastewater treatment is an energy-consuming process 40 whose approximately half of energy is being utilized in aeration processes [3, 6]. Water is an 41 essential commodity for the survival of life on earth and it has been polluted due to anthropogenic 42 activities, azo dyes and carcinogenic elements discharged through industries that affect human 43 health and the ecosystem on a large scale.

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45 Crucial and irrevocable health and environmental concerns are by highly substituted stable and 46 recalcitrant aromatic rings of azo dyes even at ppm levels in the effluent [7]. In the coming years, 47 the problem of water scarcity will be faced by all countries that induce the use of wastewater as 48 valuable energy and water resource [8]. Of all the energy sources for next generation, microbial 49 fuel cell (MFC) is getting worldwide attention The expanse of consideration in MFC to associate 50 wastewater treatment and biological power production is a substantial approach for sustainable bio-electrochemical system [7, 9]on account of its ability to treat wastewater and generate energy in the form of electric current simultaneously. These are the fuel cells that harvest chemical energy from organic matter present in wastewater and transform them into electrical energy with the aid of microbes [10]. In contrast to the conventional fuel cells, expensive metal catalysts are not utilized in MFCs.

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57 Hence, this technology signifies a new approach using inexpensive ion exchange membranes and 58 binders to generate electric current [11]. Heavy metal pollution due to the untreated wastewater 59 emerging from industries has become one of the major environmental issues. This matter is of 60 utmost importance because of the recalcitrance, toxicity and persistence of these heavy metals. In 61 the past few years, several physical, chemical and biological treatment methods have been applied 62 for heavy metal removal from wastewater including adsorption, chemical precipitation, 63 flocculation and technologies based on electrochemical treatment [12]. The production of toxic 64 chemicals, by-products and more sludge production is the limitation of these methods. Immense 65 attention has been paid to induce such a novel approach for heavy metal recovery that is both eco-66 friendly as well as economical [13]. Using different electron acceptors in the cathodic chamber, 67 the reduction of metals occurs and at last, can be recovered from the surface of cathode [14]. 68 Numerous industries including textile and pharmaceutical drain out wastewater without any 69 preliminary treatment process causing some diseases including ischaemic heart disease, chronic 70 obstructive pulmonary disease, lung cancer and many environmental problems because of the 71 presence of carcinogenic elements such as chromium, lead and arsenic and dyes which need to be 72 degraded.

74 Among all industries, the most polluting industry is the textile industry where dyes are used for 75 the colouration of fabrics and the waste materials consist of heavy quantities of azo dyes polluting 76 the whole environment on a large scale Azo dyes contribute the largest production volume, 77 approximately 70%, to dye industry [15]. Low light penetration, high chemical oxygen demand, 78 increased chromaticity and grievous environmental pollution are the characteristics of azo dyes 79 contaminated wastewater [16]. Regarding the extensive use and their chemical structures, dyes 80 have been categorized into five major branches which are; basic, acidic, reactive, direct and 81 disperse dyes [17]. The most frequently and predominant organic dye present in industrial 82 wastewater is azo dye which is chemically a compound having a nitrogen-nitrogen double bond (-83 N=N-) and because of its complicated framework, it is difficult to be reduced. However, these 84 dyes are easily decolourized by acquiring electrons being released from organic compounds 85 oxidation process [18, 19]. The chromophoric group is azo group i.e. colour generating constituents imparting a specific colour to the dye. Along with this group, the phenomenon of 86 87 resonance is shown by delocalized electrons of p-orbitals in the benzene ring.

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89 The presence of different chemical substituents with the azo bond would alter the properties of the 90 dye. Microbial fuel cell (MFC) represents a promising bio-electrochemical technology that makes 91 use of microbial catalytic activity to extract chemical energy stored in organic matter and convert 92 into electrical energy [20-24]. Microbial fuel cell (MFC) has proved to be an excellent emerging 93 approach because of its cost-effectiveness and sustainability to harvest electrical energy from 94 wastewater [25]. In general, MFC is comprised of an anode and a cathode chamber (Fig. 1) in 95 between which a proton exchange membrane is inserted to avoid the diffusion of electrolytes 96 between two compartments [26].



Fig. 1. Schematic representation of typical Microbial Fuel Cell [27].

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100 Electrons and protons are generated in the anode chamber through oxidation of organic substances 101 owing to the catalytic activity of bacteria. Electrons then move towards the cathode electrode 102 through external circuit connections while protons move through proton exchange membrane [28-103 30]. In the cathodic compartment, a reduced compound or water is produced due to the reaction of 104 electrons and protons with oxygen or any other compound serving as a terminal electron acceptor. 105 Electric current is generated on account of the utilization of electrons moved from anode to cathode 106 through external connection. Different kinds of wastewaters having variable compositions are 107 utilized as fuels and treated in microbial fuel cells such as industrial, domestic and agricultural 108 wastewaters [31-37].

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The performance of MFC is affected by bacterial adhesion, electron transfer and electrochemicalefficiency which rely upon the selection of adequate electrode material. The efficacy of MFC can

112 be improved by an increase in the surface area of electrodes to offer more reaction sites, reduction 113 in porosity to enhance electrical conductivity, the use of 2D-nanomaterials can expand the domain 114 of electro-microbiology [38, 39], high electrical conductivity and low interfacial impedance to 115 facilitate the flow of electrons in external circuit with least resistance [40] [41], fouling and life of 116 electrodes can be controlled by selection of materials resistant to acids and bases and for 117 commercial purposes, the material should be low cost. Moreover, the supercilious biocompatible 118 electrode material improves bacterial adherence and life of MFC Electrode materials for microbial 119 fuel cells: nanomaterial approach, Mater Renew Sustain Energy [42] To scale up the efficiency of 120 MFC, a number of studies are reported with different electrode materials; activated Carbon [43] 121 carbon cloth dopped with nitrogen gas [39], carbon-based plain carbon paper [44] granular 122 graphite [45], metal and metal oxides [46] [47] and composites [48].

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124 The performance of MFCs has been examined by changing the configurations, substrate material, conditions of operation and indicators. The variability in each of these key parameters significantly 125 126 affects the efficiency of treatment and generation of electric power. Many ongoing researches on 127 microbial fuel cells have shifted their attention from batch lab-scale configurations towards 128 continuous-flow scalable setups of MFCs. This necessitates a complete thoughtful of the separate 129 and mutual effects of operating conditions and configuration of the reactor. Scaling up can be done 130 by piling up multiple cells, more than one electrode in the same cell or by increasing the size of 131 the cell [49]. MFC seems to be a promising approach from both financial and environmental 132 aspects [50, 51]. The ultimate goal of this present review is to conclude various key parameters, 133 different designs and electrode materials with little modifications best suited to the performance 134 of cells in terms of power generation and treatment efficiency.

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136 The purpose of a model is to replicate the performance of a system employing a set of laws and 137 equations, to study the density and steady/dynamic nature of the MFC poses boundaries. Dynamic 138 and steady-state 1-D, 2-D and 3-D models for simulation of MFC have been studied and intricacy 139 of the model depends upon dimensions of coherence and established assumptions [52]. [38] 140 studied one-dimensional modelling and simulation by Solid Edge. Electrochemical behaviour of 141 MFC can be studied by various numerical expressions/laws like Ohm's law, Nernst-Monod 142 expression to describe the rate of electron-donor (ED) oxidation [53], Butler–Volmer expressions 143 [54] finite volume method/finite difference method/ parallel computation/ multiple step times and 144 computational fluid dynamics method, Nernst-Planck equation [55].

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146 Electrode materials play an inevitable role in the power output and cost of MFCs, to convert 147 chemical energy into electricity by employing bacteria to oxidize organic/inorganic matter. In this 148 paper, the recent progress of anode/cathode materials for MFCs has been scientifically swotted, 149 subsequently detailed insights into the characteristics, some prevailing problems, advancements, 150 assessment parameters of the electrode materials and their effectiveness in terms of wastewater 151 treatment. It is observed that the difference in materials of electrodes resulted in a significant 152 difference in the output and electrode modifications came out to be a promising substitute to 153 upscale the efficacy of MFCs. From the perspicacity of recent developments, the exploration of 154 electrode materials will be very imperative and vendible as an affordable price and exceptional 155 performance will significantly outspread the application of MFCs.

157 However ongoing studies at electrode modification have substantially upgraded the performance 158 of MFCs, at present the working mechanism in most of the studies, still demands more workforce, 159 which is not very clear. For this promising wastewater treatment technology, durability and long-160 working life of electrode materials are unavoidable aspects. Unfortunately, most of the present 161 studies remained heedful to the performance/output power, not copiously addressing the stability 162 of the electrode materials, which would eventually lack to offer a valuable standard for their long-163 term provision in industrial application. This review is novel in respective of an assemblage of 164 recent advances in electrode fabrication strategies analyzing MFCs performance with reference to 165 electricity generation and it highlights the crucial need for extensive studies on the working 166 mechanism of electrodes other than improving their operational life to improve the durability of 167 MFCs.

168 **2 Microl**

2 Microbial fuel cells (MFCs)

169 Wastewater treatment has become a major global concern these days on account of a tremendous 170 increase in industrialization and anthropogenic activities causing various health issues. Error! 171 **Reference source not found.** represents the schematic overview of anaerobic treatment that 172 majorly produce biogas, effluents and sludge. The industrial waste containing hazardous chemicals 173 and dyes is discharged into water bodies without being given any preliminary treatments. When 174 sustainable energy resources come under discussion, we talk about technologies that are pollution-175 free and non-combustible [56]. The inadequacy of water supply is predominantly contributed by 176 wastewater generated from domestic as well as industrial sources [57]. This led to the treatment of 177 wastewater before ejection in the environment by applying various expensive chemicals [58, 59]. 178 Therefore, we need such sustainable energy sources as alternatives inducing a less hazardous 179 environment.



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Fig. 2. A Scheme of anaerobic wastewater treatment.

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183 In the coming years, one cannot be dependent merely upon fossil fuel energy due to a drastic 184 increase in the energy crisis, hence we need renewable energy resources. To cope up with the 185 problems relevant to wastewater drained out by textile industries, a new biological approach and 186 an emerging technology under consideration is a single-chambered microbial fuel cell (SCMFC) 187 which treats wastewater and simultaneously converts chemical energy through oxidation into 188 electricity due to catalytic activity of microbial community [60]. MFC has gained much attraction 189 due to its environmental profits. This technology discovers the metabolic reactions of different 190 microbial species such as Shewanella sp., Geobacter sp., yeast and consortium of species that help 191 in catalysis of redox reactions [61]. In MFC, electrons are emitted through oxidation of organics

at the anode via electrogenic microorganisms, which then combine with diffused protons atcathode and electricity is generated through reduction reaction [62].

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195 MFC is a biological approach that not only raises power generation standards but also addresses 196 fuel economy by the utilization of domestic and industrial wastewater. This system generates 197 power along with wastewater treatment leading to a sustainable future that can use non-fossil 198 resources for power generation [63]. In general, power is generated owing to the metabolism of 199 bacteria that produce electrons by consuming the substrate present as contaminants in wastewater 200 inside MFC and these electrons then complete the reaction by moving through an external circuit 201 towards the cathode [64]. As the electrons are only produced from bacteria, so the thickness of 202 active biofilm growth on the anode is responsible for the extent of generated electric power [65]. 203 The cell performance is affected by the significant contribution of many factors including the 204 oxygen received by cathode compartment, substrate oxidation in an anodic compartment, 205 movement of electrons towards anode surface and extent of proton diffusivity through the cation 206 or anion exchange membrane [66].

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Advantages linked to the use of MFCs are the lower yield of sludge to be disposed of and no need for aeration as compared to other conservational techniques. The process of electricity generation through MFCs is clean and further does not need any kind of purification process, as in the case of hydrogen and methane produced under anaerobic conditions [67]. In future, an increase in wastewater emitting from industries and houses which is estimated to be 7% per year would need more energy resources for the treatment. Vast research has been carried out to produce electricity simultaneously with the treatment of wastewater using MFCs generating current densities within 215 $0.06 - 1000 \text{ mA/cm}^2$ range [31, 68]. Recently, the MFC system was used not only to generate the 216 power density but also to effectively remove the chemical oxygen demand (COD). The two 217 different MFC reactors were analyzed and the results showed a maximum power output and COD 218 removal with R_{cc} MFC reactor at the concentration of 2900 mg/L (Fig. 3). The greater efficiency 219 of R_{cc} MFC reactor was attributed to the high external load in closed circuit, greater metabolic 220 activity and maximum breakdown of the substrate [69].



Fig. 3. (a) Efficiency correlation of actual and predicted COD removal, (b) pH and reaction time response surface plot for COD removal, (c) combined effect plot between concentration and reaction time on COD removal [69].

225 **2.1. Electron transfer mechanism in MFCs**

226 Bacterial strains generate electrons via various bio-electrochemical processes (Error! Reference 227 source not found.), and a specific mechanism is developed for extracellular electron transfer 228 (EET). These systems involve the use of electroactive species that catalyze redox reactions at 229 cathode and anode having the unique capability of transforming chemical energy of wastewater 230 pollutants into bioelectricity or some other valuable products or hydrogen in microbial electrolysis 231 cells (MEC). Pure anaerobic strains called exoelectrogens transport electrons from the oxidation 232 product to the electrode with the aid of projected nanowires, external mediators or specific 233 proteins. Many strains have been investigated for their potential to produce more power in MFCs. 234 The bacteria can transfer electrons to the electrodes by three principal mechanisms. Fermentative 235 bacteria, in an indirect MFC, yield end products like hydrogen, carbon dioxide, alcohols, or 236 ammonia. Under anaerobic conditions, these reduced products are formed when the electron 237 produced through substrate breakdown is used to reduce some intermediate products like proton 238 or alcohol.

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240 Therefore, these fermentative bacteria are not able to donate the electrons to anode, so to make use 241 of these bacteria, external mediators are which can shuttle between cell membrane and anode. The 242 bacterial strains which need mediators for electron transfer include *Streptococcus lactis*, *Proteus* 243 *mirabilis* and *Klebsiella pneumonia* while the bacterial strains that do not require any mediator 244 include Aeromonas hydrophila, Geobacter metallireducens, Rhodoferax ferrireducens and 245 Geobacter sulfurreducens. Recent studies revealed that some species can perform in the absence 246 of any mediator, but if they are added, their efficiency can be improved such as Shewanella 247 putrefaciens [70]. Another extracellular electron transfer mechanism includes the use of redox

248 mediators for shuttling of electrons. A mediator should exhibit a few salient features like the ability 249 to develop a physical attachment with the electrode surface, electrochemically active, should have 250 low oxidation potential, should not absorb on the surface of bacteria or electrode.



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Fig. 4. Electron transfer mechanism in a microbial fuel cell.

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254 The oxidation potential of the mediator should be closer to the redox potential of the primary 255 substrate. The mediator can be membrane-bound or soluble in the medium [71]. Some commonly 256 used natural/synthetic electron mediators ferrying between inside cell membrane of bacteria and 257 anode are Phenazine ethosulphate, 2-hydroxy-1,4-naphthoquinone, gallocyanine, benzylviologen, 258 2,6-dichlorophenolindophenol, antraquinone-2- disulfonate, and thionine [72]. Generally, it is 259 known that electroactive bacterial strain Geobacter sulfurreducens directly transfer electrons with 260 projected appendages named as nanowires. The direct transference of electrons, produced through 261 respiration from the electroactive bacteria to the anode is the third and the most significant 262 mechanism. it was first projected that microbes can transfer electrons to an electrode surface when 263 strains of *Shewanella putrefaciens* during metabolism of lactate generated electricity [73]. The

264 metal-reducing bacterium *Shewanella putrefaciens* were found to have cytochromes (electron 265 carriers) in its external membrane and were capable of generating anodic current in the absence of 266 terminal electron acceptors. The selection of mechanism mainly depends on the microbial potential 267 for EET and the type of environmental pollutant to be removed [74].

268 **3** Configurations of microbial fuel cell

Generally, a microbial fuel cell is comprised of an anodic compartment, cathodic compartment, proton exchange membrane or salt bridge and assembly of electrodes. The classification of microbial fuel cells was done based on the mode of operation and design [75].

272 **3.1 Dual-chambered**

273 A dual-chambered MFC (Error! Reference source not found. (B), as the name implies, consists 274 of an anode and cathode that are separated by placing a salt bridge. This is basically H type design 275 of MFC (Error! Reference source not found. (A)). Microbes, media solution and electrodes are 276 present in the anode chamber while fresh water and electrode are contained within the cathode 277 chamber having a supply of oxygen from the surrounding. In Fig. 5(A), the circular orientations 278 around anode compartment are representing microbial growth and biofilm production. The major 279 limitation associated with the less efficiency of this configuration is the increase of internal 280 resistance due to increased distance between the electrodes. Commonly used electrodes are made 281 of graphite, copper, stainless steel mesh, carbon paper and carbon cloth [76].



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Fig. 5. (A) Working of dual-chambered cell, (B) Dual-chambered, (C) Working of singlechambered cell and (D) Single-chambered cell.

285 **3.2 Single-chambered**

286 The second configuration of MFC is single-chambered (Error! Reference source not found. (D)) 287 that is composed of an anode chamber only and the cathode is faced towards the atmosphere 288 (Error! Reference source not found. (C)). Active aeration is not compulsory in this 289 configuration. This is a simple design that can be functioned in two modes i.e., batch or 290 continuous. The design is cost-effective and because of its simplicity, scaling up the process is 291 very easy. This cell configuration is efficient and preferred due to lower internal resistance in 292 comparison to dual-chambered MFCs. The main advantage associated with the use of single-293 chambered MFC is cost-effectiveness along with the generation of more power output [76].

294 **3.3 Up-flow MFC**

The up-flow configuration is made in such a way that wastewater is entered from the bottom and effluent is pumped out from the top side. The mode of operation in this configuration is continuous [77].

298 **3.4 Stacked MFC**

As the name indicates, stacked MFC is comprised of many microbial fuel cells connected in either series or parallel combinations to obtain high power output. Different studies conducted on stacked MFCs revealed parallel combination to be more efficient than series combination [2].

302 3.5 Paper MFC

The material used for the fabrication of electrodes in this type of MFC was paper having the benefits of being cost-effective and chemical-free. The design is simply comprised of an anode and cathode [78].

306 4 Electrode fabrication

307 Many factors affecting the cell performance include the type of substrate, pH, temperature, 308 electron transfer mechanism opted by microbes, the configuration of the cell, membrane and the 309 material of electrode [79]. The fabrication of electrodes is the major factor having a dominant 310 effect on the working of MFCs. Many researchers have now shifted their attention towards 311 materials of the electrode as the performance is directly dependent on the electrode kinetics [80]. 312 The selection of anode material has a significant impact on the performance of microbial fuel cells 313 in terms of treatment efficiency, adhesion of microbes to the electrode and the transference of 314 electrons from microbial appendages to the electrode surface [81]. Therefore, the materials for the 315 construction of anode should possess some specific properties that not only improve the adhesion

316 capacity of electroactive bacteria on the anode and the movement of electrons towards the 317 electrode surface but also the collection of current. A number of anode materials including carbon 318 and metal-based with different modifications have been assessed to enhance the performance of 319 the cell [82].

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321 The most commonly used materials for anode fabrication were carbon-based because of its several 322 characteristics such as high conductivity, chemical stability and biocompatibility. Numerous 323 carbon-based materials have been utilized as anode electrodes including graphite rods [83], carbon 324 felt [84], carbon cloth [85], carbon mesh [86], carbon brush [87], carbon veil [88]. In contrast to 325 that, bacteria cannot grow on the surface of metals due to their antimicrobial activity but this 326 characteristic is not present in electrogens having the capability to generate a highly active biofilm 327 on the electrode surface [89]. One of the mechanisms for the fabrication of hybrid G-CNT biofilm 328 is shown in Fig. 6. According to this process, carbon nanotubes can easily bind with the graphene 329 oxide sheet and by incubation of the microbes, sheets turn into biofilms. These biofilms with 330 enhanced microbe loading then successfully transfer electron direct to the electrodes via OM c-331 Cysts [90]. Instead of biofilms, now metal-based materials can also be used in MFC. The main 332 advantage of using metal-based electrode materials is high conductivity, robustness and 333 inexpensiveness as compared to carbon-based materials [8, 91].





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Fig. 6. Fabrication and electron transfer process of hybrid G-CNT biofilm [92].

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337 The type of cathode used is a major hindrance significantly affecting the performance of the cell. 338 To manufacture a cathode that is cost-effective and generates maximum electric power and 339 columbic efficiency is the most challenging part in this technology to be applied successfully 340 specifically for wastewater treatment [66]. Along with robustness, a good cathode must possess 341 some specific properties such as catalytic, high conductivity and mechanical stability [80]. Fig. 7 342 explains the fabrication process of rGO-AC cathode. The rGO-AC equipped cathode utilized in 343 the single-chamber MFC device is not only potentially affordable but also gives the maximum power density of 2.25 W/m² [93]. Most of the materials used for the fabrication of anodes in MFCs 344 345 have also been utilized for the construction of cathodes. The most widely used catalyst for the 346 cathode is platinum. Cathodes have been classified into two categories i.e., biotic and abiotic 347 cathodes while biocathodes can be further either aerobic or anaerobic [94].



Fig. 7. (a-c) Schematic representation of the fabrication process of rGO-AC. (b) Final diagram of fabricated rGO-AC cathode [93].

4.1 Terminal electron acceptor in cathode

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352 Electrons are released from the degradation of organic matter which eventually travels towards the 353 cathode to be finally oxidized by the aid of electron acceptors [95]. Much attention has been paid 354 to the substrate employed in the anodic chamber while studies are less focused on the terminal 355 electron acceptors in the cathode chamber in spite of their significant impact on the cell 356 performance. A good electron acceptor must have high reduction potential and fast kinetics along 357 with its availability, cost-effectiveness and stability [96]. Up to now, oxygen has been regarded as 358 the most useful and frequently utilized electron acceptor on account of its characteristics of high 359 oxidation potential, availability and the production of clean water after the reduction process [97]. 360 But many studies have reported this oxygen supply to the cathode as a power-consuming process 361 [10, 98]. To cope up with the need for some other electron acceptors having varied redox potential 362 and to make cathodic reactions more effective, studies are being conducted to assess the feasibility 363 of altered electron acceptors [14]. The most commonly used electron acceptors in addition to 364 oxygen are ferricyanide [99-101] and permanganate [102, 103].

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366 You et al. [102] concluded that power density with permanganate was higher (116 mW/m²) in 367 comparison to ferricyanide (16 mW/m²). Microbial fuel cells (MFCs) have been studied 368 frequently by many scientists and different modifications have been done to commercialize it on 369 a large scale to produce more power with efficient fuel consumption. The biofilm used at the anode 370 performs a dual function of pollutants degradation, generation of power and producing 50-90% 371 less disposable solid residue [15]. Based on the kind of microbes used in MFC, the biological 372 approach for azo dye degradation can be aerobic, anaerobic or a mixture of both conditions [104, 373 105]. Some researchers [106] recently evaluate the aerobic and anaerobic degradation by adopting 374 iMFC and dMFC systems (Fig. 8). Both of them successfully process biodegradation and revealed 375 comparative results. Table 1 summarizes maximum power output and colour removal efficiencies using different configurations of MFCs for different azo dyes. 376



Fig. 8. Proposed aerobic and anaerobic biodegradation pathway of 2,4- DCP. Proposed reactions
 in roman number represent reductive dehalogenation, decarboxylation and aromatic ring cleavage
 [106].

| MFC type | Dye/s | Concentration (mg/L) | Anode – Cathode | Power output | Colour removal (%) | References |
|---|--|-------------------------|--|---|-----------------------|------------|
| H-shaped MFC | Methyl orange, congo red, Reactive blue 172, reactive | | Graphite based Metal salt - GECE | $\begin{array}{c} \mbox{Methyl orange} - 4100{\times}10^{-6} \\ \mbox{W/m}^2 \end{array}$ | 94 | [107] |
| | yellow 145 and reactive red 2 | | | $\begin{array}{c} MO-4676{\times}10^{-6}~W/m^2 \\ RB-2593{\times}10^{-6}~W/m^2 \end{array}$ | 90 | |
| Planted CW-MFC | Reactive brilliant red X-3B (ABRX3) | | Granular Activated Carbon | 0.3 W/m ³ | 91 | [108] |
| Pilot-scale anaerobic baffled reactor with biocatalyzed electrolysis system | Alizarin yellow R (AYR) | 200 | Granular graphite | - | 96 | [109] |
| Single-chambered | Thionine-based textile dye | 40 | Porous carbon cloth (anode) and PTFE diffusion layer (cathode) | $83 \times 10^{-3} W/m^2$ | - | [110] |
| Constructed wetland – MFC | Reactive brilliant red X-3B (ABRX3) | 300 | Activated carbon and stainless steel mesh | 0.9 W/m ³ | 96 | [111] |
| Single-chambered up-flow | Acid orange 7 (AO7) | - | Carbon felt and carbon plate | - | 81 | [77] |
| Single-chambered | Orange I, II and methyl orange | - | Carbon felt | - | | [112] |
| Air-cathode single-chambered MFC | Active brilliant red X-3B (ABRX3) | 100 | Porous carbon papers & Pt- coated air cathode with PTFE layer | $373 \times 10^{-3} W/m^2$ | 90 | [113] |

Table 1. A comparison of maximum power output and colour removal efficiencies of various microbial fuel cells.

| Air-cathode single-chambered MFC | Active brilliant red X-3B (ABRX3) | 300 - 1500 | Porous carbon papers & Pt- coated air cathode with PTFE layer | $274 \times 10^{-3} W/m^2$ | 90 | [114] |
|--|-----------------------------------|------------|--|--|---------|-------|
| Anaerobic-aerobic sequential reactor and MFC coupled | Congo red | 100 | Plain carbon felt (anode) and graphite-granules (cathode) | | 93 | [115] |
| Single-chambered biocathode- MFC | Azo dye | | Granular activated carbon | 8 W/m ³ | 75 | [116] |
| Biocathode-MFC | Congo red | 300 | Porous carbon papers | $9 \times 10^{-3} W/m^2$ | | [117] |
| Dual-chambered | Orange G | - | Graphite rods | $91 \times 10^{-3} W/m^2$ | - 97 | [118] |
| Dual-chambered | Reactive blue (RB221) | - | Modified graphite electrode | $21 \times 10^{-3} W/m^2$ | 74 | [119] |
| Single-chambered air cathode | Congo red | - | Graphite felt (anode) and Pt- coated carbon paper (cathode) | $53 \times 10^{-3} W/m^2$ | 90 | [120] |
| Biocathode with dual- chambered MFC and air- cathode with single-chambered | Congo red | - | Non-wet proofed porous carbon paper and Pt- coated wet-proofed PCP | $324 \times 10^{-3} W/m^2$ | 96 | [121] |
| Dual-chambered MFC (saline catholyte) | - | - | Graphite fiber brushes & Pt- coated wet-proofed CC | $491 \times 10^{-3} W/m^2$ | - | [122] |
| Air-cathode buffer-free MFC | | | Graphite felt & activated carbon air-cathode | $512 \times 10^{-3} W/m^2$ | - | [123] |
| Continuous-flow MFC | X-3B | 200 | Air-cathode | Decreased slowly with increased operational time | - | [124] |
| Dual-chambered | Reactive blue 19 (RB19) | 50 | Carbon felts | - | 89 | [16] |

| Single-chambered | - | | Cu ₂ O nanoparticles/graphene oxide and Pt/C as cathode catalysts | - | - | [62] |
|----------------------------------|----------------------------|-----------|--|-----------------------------|----|-------|
| Two rectangular perspex frames | Acid Orange 7 | 0.06 | Granular graphite | 0.31 W/m ³ | - | [125] |
| Air-cathode single-chambered | Reactive blue 160 (RBu160) | 450 - 560 | Activated and hydrophobic carbon cloth | $197 \times 10^{-3} W/m^2$ | - | [126] |
| Dual- chambered | Methyl orange | 10-20 | Rutile-coated graphite | - | 73 | [127] |
| Air-cathode single-chambered | Congo red | 300 | Porous carbon papers | $192 \times 10^{-3} W/m^2$ | 90 | [128] |
| Dual-chambered | Congo red | 300 | Carbon paper electrode | 214 mV | - | [129] |
| Dual-chambered | Congo red | 300 | Porous carbon papers | 0.25 V | 95 | [130] |
| Dual-chambered | 4-Nitrophenol | 139,00 | Carbon felt | $143 \times 10^{-3} W/m^2$ | - | [131] |
| Cylindrical single-chambered MFC | Acid Orange 7 | 70-210 | Carbon fabric | - | - | [132] |
| Dual-chambered | 1,2-Dichloroethane | 102 | Graphite granules | - | 43 | [133] |

383 Some microbial communities Geobacter sulfurreducens and Beta Proteobacteria were also used 384 in mediator-free planted CW-MFC to examine electricity production and dye degradation [108]. 385 A *Pseudomonas*-catalyzed microbial fuel cell was designed to examine the degradation of various 386 dyes including reactive blue 172 (RB), methyl orange, Congo red, reactive red 2 and reactive 387 yellow 145, which have capability to form electron-shuttling substances [107]. Alizarin yellow R-388 bearing wastewater treated in anaerobic baffled reactor coupled with bio catalyzed electrolysis 389 system (ABR-BES) containing sludge from wastewater plant exhibited colour removal up to 96% 390 and generated current output of 24 A/m³ [109]. Rather than using a single bacterium for the 391 removal of dyes from wastewater, a more pragmatic approach to make use of sludge emerged with 392 promising results. Anaerobic sludge collected from municipal wastewater for decolourization of 393 commercially used reactive and azo dyes (brilliant red, acid orange 7, congo red) MFC coupled 394 constructed wetlands (CW-MFC) showed significant colour removal efficiency (more than 80%) 395 [55, 90, 99].

396

397 In view of flexibility in regulating the pH, phosphate buffer is popularly used as a catholyte [134]. 398 Electricity generation was enhanced by short-term adjustment of pH of anolyte in anodic 399 compartment leading to increase of electroactive bacteria (EAB) biofilm formation from 59 to 400 75% triggering an acceleration of redox reactions and decrease in resistances of electrodes but it 401 is not advantageous on a large-scale [123]. Disadvantages related to the use of glucose is 402 methanogenesis and fermentation causing the inhibition of electricity production, as well as regular 403 replacement of the medium, which also results in less power output [92]. In single-chambered 404 MFC, Kalathil et al. [116] revealed a power output of 8 W/m³ by using graphite-activated carbon 405 (GAC) as biocathode. The associated advantages are that pH adjustments and preheating process

406 are not required. Fang et al., [108] reported 91% decolourization of dye (ABRX3) in planted MFC
407 generating a voltage of 610 mV when GAC anode/cathode was used.

408

409 The design of such a microbial fuel cell that can be commercialized on a large scale is still a 410 challenge to be accomplished. It is essential to find out the power generation with dye 411 decolourization efficiency. A single-chambered air-cathode MFC was used to decolourize active 412 brilliant red X-3B for the first time by Sun et al [114] resulted in 90% colour removal with power 413 generation of 274 mW/m² when glucose was used as an organic substrate. In contrast to that, an 414 attempt was made by Liu et al. [112] to decolourize orange I, orange II and methyl orange in the 415 presence of phosphate buffer in the cathodic compartment and the results indicated a complete 416 reduction of dyes with voltage generation of 282 mV utilizing glucose in the anodic chamber. 417 [113]. Li et al. [115] have discussed the step by step mechanism of azo dye degradation in an 418 anaerobic-aerobic sequential MFC reactor, describing the cleavage of azo bond in anode chamber 419 under anaerobic situation and reduction into aromatic amines and dissociation of these amines 420 under an anaerobic situation in the cathodic compartment, but its maintenance is difficult with a 421 continuous mode of action.

422

423 MFC exhibited substantial performance while exploiting enzymatic oxidation in cathode 424 compartment in terms of decolourization [119]. Another design of MFC was developed for the 425 removal of commercially used dyes by the name of constructed wetlands MFC (CW-MFC) which 426 attained extensive decolourization with efficient power output [108, 109]. The colour removal of 427 active brilliant red (ABRX3) and maximum power output reported to be 93% and 0.06 W/m³ 428 respectively in cylindrical planted constructed wetlands MFC [111]. A green approach was used for the generation of electricity from waste and results described those pure strains were less productive than mixed cultures and MFC using Pt as catalyst exhibited 16 times more power density compared with MFC without the catalyst. But the Pt catalyst cannot be used because of its high cost. In MFCs, the microbial communities in anode and cathode chambers were quantified using various gene sequencing techniques including 16S rRNA gene sequencing, next gene sequencing and fluorescence in-situ hybridization (FISH) which makes use of specific probes to quantify the specific populations [135].

436

437 Electricity generation evaluated by comparing the efficiencies of Cu_2O was 438 nanoparticles/graphene oxide and Pt/C as cathode catalysts in single-chambered MFC and the 439 results depicted the highest voltage output (0.223 V) and columbic efficiency (93%) using Cu₂O 440 nanoparticles/graphene oxide. The relative abundance (49%) of microorganisms Geobacter 441 sulfurreducens in the anode with Cu₂O nanoparticles/graphene oxide was higher as compared to 442 commercial Pt/C (32%) [62]. Electron exchange is strongly based on material conductivity, 443 characteristics of the surface according to the type of microbes used in MFC being the composition 444 of an electrode a deciding factor for the implementation of MFC on a large scale [15].

445

A plain carbon felt was used as electrode material by Li et al. [115] which resulted in colour removal of Congo red dye to be 93% along with 95% COD removal of wastewater generated a maximum voltage of 360 mV. By increasing the surface area of the anode from 18 to 36 cm² comprising of porous carbon papers, the colour removal of Congo red was raised to 163%, apart from that, decolourization time declined from 168 to 72 h. In addition, increasing the surface area of the anode by four times (72 cm²) caused complete removal of dye within 26 h [136]. Graphite 452 granules showed conductivity, but the drawback was the formation of clogs in the system. To sort 453 out this problem, a cuboid basket composed of titanium made by Cui et al. [109] was compactly 454 filled with graphite granules and a titanium rod was utilized to establish a connection with an 455 external circuit. In this configuration, the large surface area of granules provided maximum colour 456 removal of alizarin yellow azo dye and voltage simultaneously.

457 **5** Assessment of parameters effecting power output of MFCs

458 Several parameters affect the performance of MFC including the type of substrate to be added for 459 consumption by electroactive microorganisms, temperature maintained in the cell, pH variations 460 due to anolyte and catholyte composition and hydraulic retention time (Fig. 9) [49].



461

462 **Fig. 9**. Summary of parameters affecting the performance of microbial fuel cells.

463 **5.1 Effect of substrate**

464 The substrate origin plays a vital role in power production by MFC. Many organic materials e.g.,

465 glucose, acetate and lactate can be utilized as substrates for microbes. Some organic compounds

466 present in wastewater can also be consumed by microbes as energy sources. Acetate is frequently 467 employed due to stability in its nature and showed approximately 66% higher efficiency in 468 comparison to butyrate [137]. Sodium acetate has generated power output of 308 mW/m² and COD 469 removal up to 99% [138, 139]. More the amount of substrate available for oxidation by microbes, 470 more electrons will move through the external circuit and hence more electricity generation. All 471 substrates exhibit different efficiencies to get oxidized in an anodic chamber from which acetate 472 depicts the highest conversion efficiency of 72% [75].

473 **5.2 Effect of temperature**

474 Cell thermodynamics, reaction kinetics and microbial community are significantly affected by the 475 temperature maintained inside the MFC. The temperature between 20–30 °C has been adopted in 476 most of the studies because of the maximum microbial activity in this range. [86]. The performance 477 of the cell was reduced at lower temperatures. The power output was increased by 10% in an 478 experiment conducted at a temperature ranging from 17–22 °C [140]. An exponential relationship 479 instead of a linear was observed between temperature and power density. Increased temperature is 480 favourable for microbial growth and its catalytic activity. A urinal system based on the use of 481 undiluted urine for COD removal and current production was powered by taking on a stack of 482 MFCs and the power density was observed to be enhanced on increasing the temperature [141].

483 **5.3 Effect of pH**

484 pH is another key parameter playing a vital role in the performance of MFC. The main challenge 485 is to maintain both anodic and cathodic compartments at a specific pH. The generation of protons 486 in the anodic chamber leads to a decrease in pH and these protons then migrate from anode to 487 cathode through proton exchange membrane. It is important to be stated that this pH difference 488 will affect the stability and performance of the system [66]. The higher the pH, the lesser the 489 number of protons will migrate towards cathode chamber leading to the inefficient reduction 490 reaction hence affecting the performance of MFC. Weakly alkaline and neutral pH is regarded as 491 beneficial for biofilm growth on the surface of the anode electrode. It was found that the biofilm 492 growth and the power output can be promoted through short-term pH adjustment of anolyte 493 solution [123]. Another key factor contributing to the working of MFCs is the composition of the 494 cathode electrode responsible for reduction reaction by capturing the protons. Oxygen is the major 495 electron acceptor used in MFCs. Different types of cathodes have been used by scientists including 496 biocathodes which catalyze the reduction via microorganisms in the cathode chamber and directly 497 capture the electrons [142]. A biocathode MFC depicted brilliant performance in decolourization of Congo red dye within 48 h with a maximum power output of 9mW/m^2 . The highest 498 decolourization of 94% and power output of $4100 \,\mu W/m^2$ was observed in the case of methyl 499 500 orange in MFC containing graphite electrodes [107]. Table 2 summarizes cathodes with variable 501 composition generating power output using biocatalyst in various conformations of the microbial 502 fuel cell.

 Table 2. Summary of various developed cathodes generating power output.

| Conformation of | Strain | Cathode composition | COD removal | Power output | References |
|----------------------------------|------------------------------|--|----------------|---|------------|
| MFC | | | (%) | | |
| Single-chambered | - | Plain carbon rods | 92 | 165 μA 302 mV | [143] |
| Single-chambered | Bacillus firmus – NMBL-03 | Graphite | - | 2.9 mW/m ² | [144] |
| Double-chambered | - | PVDF coated activated carbon cloth | 64 | 110 mW/m ² | [63] |
| Single-chambered | - | Activated carbon cathode having carbon black | > 60 | 430 mW/m ² | [64] |
| Dual-chambered | Pseudomonas | Carbon felt | - | 0.32 mW | [145] |
| Dual-chambered | - | Biocathode | - | Lower than air cathode | [121] |
| Single-chambered | - | Platinum coated on air- cathode | - | - | [121] |
| Double-chambered | - | Plain porous carbon papers | - | 0.25 V | [130] |
| Double-chambered | Geobacter | Carbon cloth | 66 - 86 | 3.5 A/m ² 1.62 W/m ² | [146] |
| Serpentine up-flow | - | PVDF-based activated carbon air-cathode | 92 | 4 W/m ³ 5 V | [147] |
| Double-chambered | - | Graphite plates | - | 16 W/m ³ 1V | [148] |
| Single-chambered | - | PVC-co-PVP based activated carbon air- cathode modified with carbon black | 79 | 1330 mW/m ² | [149] |
| Single-chambered | - | PVDF based activated carbon | - | 1470 mW/m^2 | [150] |
| Stacked MFC | - | Granular activated carbon bed | 97% within 48h | 50 W/m ³ | [151] |
| Modularized MFC | - | Polyvinyl chloride | 70–90% | Upton 60 W/m ³ | [152] |
| - | - | Carbon felt | - | 4 W/m^3 | [153] |
| Stacked mono- chamber | - | Carbon paper with Platinum | >90% | 1150 mA/m ² | [154] |
| Double-chambered | - | Compact graphite | - | 47 mW/m^2 | [155] |
| Stacked single- chambered MFC | - | Carbon felt | - | Up to 181 mW/m ² | [156] |

505 In MFCs, proton exchange membranes like Nafion, ultrafiltration membrane, act as a barrier 506 between anodic and cathodic compartment hindering the flow of oxygen and substrates but helps 507 in the diffusion of protons towards the cathode chamber with more than 95% MFC performance 508 in terms of power output [118, 121]. Power generation in microbial fuel cells is dependent on the 509 nature of anolyte and catholyte employed and pH. For the treatment of textile effluent, dye-bearing 510 wastewater with injected biomass is the most commonly used anolyte solution used in MFCs [15]. 511 When exoelectrogenic bacteria is inoculated, the pH of buffered anolyte should be close to neutral 512 or a little alkaline for an excellent performance [146]. An improvement in columbic efficiency 513 (43–60%) was observed when saline solutions having high ionic strengths were taken [122]. 514 However, the observations indicated changes in pH but not in the conductivity of the solution. The 515 cost-effective design of MFC was established by Thung et al. [77] comprising of single-chamber 516 up-flow devoid of the membrane and the scaling-up process was easy to operate with this.

517

518 Electricity generation, characterization and structure of the microbial community in MFC was 519 investigated by executing long-term (400 days) and short-term (10 days) operation and the results 520 revealed an increased relative abundance of microbes responsible for organic degradation while 521 those contributing towards electricity generation decreased. Besides that, the removal efficiencies 522 and the power output also decreased during long-term operation because of increased resistances 523 internally [124]. Decolourization of reactive blue 19 (RB19) dye and bioelectricity generation was 524 assessed using MFC, which stated the improvement in microbial enzymatic activity through the 525 addition of a co-substrate, but the efficiency of degradation decreased with increasing 526 concentration of dye owing to the formation of some toxic intermediates which inhibited electricity 527 production. However, the degradation efficiency of 89% was achieved within 48 h in comparison to 51% degradation rate in open circuit when no resistance was applied and 55% in aerobicconditions [16].

530

531 Prasad et al. [75] reported that in contrast to butyrate, propionate and glucose, acetate is regarded 532 as the most efficient organic compound giving 66–72% yield. The factors which should be under 533 observation while working on MFC are the size of electrodes, the surface area of electrodes and 534 distance between the electrodes. Greater the surface area of electrodes, more microorganisms will 535 find a place to attach and hence more activity [157]. Many methods have been devised to remove 536 the organic and inorganic contents but all those need greater cost and high external energy. With 537 the help of MFC, the operational cost is reduced, and renewable energy is generated along with 538 the treatment of wastewater. Although a promising approach, its application on large scale is still 539 a challenge to be accomplished because of the low generation of electrical energy [62].

540

6 Conclusion and future perspectives

541 Microbial fuel cell technology is a promising approach for simultaneous wastewater treatment and 542 electricity generation. During the past few years, several advancements have been made in MFC 543 technology. The optimization of various parameters i.e., temperature, substrate and pH were done 544 to enhance the efficiency of the cell. By controlling these factors, maximum power output was 545 obtained. The central issue in microbial fuel cells is electricigens that must be of high quality to 546 enhance the performance of MFCs. Recently, many biological tools have been developed for the 547 modification of existing electricigens bearing tremendous electrochemical activities. The toxicity 548 of chemicals in MFC can also be sensed with the aid of electricigens. The power densities were 549 upgraded not only by the nature of microbial catalysts but also a significant change had been observed by the selection of materials used for electrode fabrication, the spacing between the electrodes and the conductivity of electrolytes within the chambers.

552

553 The power output and efficiency of the cell can be enhanced by using different ion-exchange 554 membranes and efficient binders in the fabrication of electrodes. The selection of substrate for 555 bacterial growth and terminal electron acceptor (TEA) in cathode chamber plays a significant role. 556 Sodium acetate as substrate and potassium permanganate (KMnO₄) solution as TEA has proved to 557 provide the increased electric current. In addition to that, this technology becomes economically 558 feasible when integrated in combination with other processes. There is a dire need to reverse the 559 energy, the foremost contributor to climate change. More than 3 billion people yet relying upon 560 unsustainable sources like timber, char, wood coal or dry manure fuel for cooking or heating and 561 renewable energy contributes only less than 20% to the total energy consumption. According to 562 an estimation, 1 MW of electrical energy and 2 MW of thermal power per hour can be produced 563 from one ton of biomass. With such promising projections, one of the objectives that demand 564 microbiology the most is escalating share of renewable energy for the global sustainable energy 565 sector.

566

Agricultural substrates/wastes and microbes are now used for the manufacture of third generation biofuels specifically bio-electricity. Exoelectrogens; microorganisms capable of extracellular electrons transfer are extensively explored in the field of MFCs. MFCs are a bio-electrochemical system possessing the potential for sustainable energy production by making use of degraded organic matter. Owing to low-energy output with a single microorganism in MFCs, a consortium is now used for higher-energy output. The best promising exoelectrogens are presently being

573 employed for bioelectricity production, foreseeing powering a NASA space mission. Renewable 574 energy is fundamentally associated with carbon capture along with storage and bioenergy is 575 substantial technology that will play a vital role in coping up with sustainable development goals 576 in the forthcoming decade. Another hopeful application of MFC is bioremediation used to monitor 577 the environmental pollutants and recovery of heavy metals. The dream of launching a large-scale 578 application of MFC can be accomplished by combining it with other processes.

579 Acknowledgments

580 The representative universities or institutes are thankfully acknowledged for providing literature581 services.

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