1	Synthesis of a novel nanocomposite based on date stones/CuFe ₂ O ₄
2	nanoparticles for eliminating cationic and anionic dyes from
3	aqueous solution
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23 Abstract

24 In this study, the date stones/CuFe₂O₄ nanocomposite was synthesized by a graft of CuFe₂O₄ nanoparticles in the surface of date stones (DS) for the removal of rhodamine B (RhB) 25 and methyl orange (MO) from aqueous solutions. The adsorption of RhB and MO on 26 DS@CuFe₂O₄ shows good agreement with second-order kinetic and Langmuir isotherm 27 models. The maximum adsorption capacity was found to be 555.56 03 mg g^{-1} and 303.03 mg 28 g⁻¹ for RhB and MO, respectively. This adsorption is spontaneous and endothermic. There is 29 excellent regeneration and high reusability of the DS@CuFe₂O₄ for the RhB and MO removal 30 in six cycles. 31

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Keywords: Dye; date stones; CuFe₂O₄; nanocomposite; adsorption

34 **1. Introduction**

Dyes are used in many industries such as textile, tannery, paper pulp, cosmetics, plastics, 35 leather, printing, rubber, food, and pharmaceuticals [1–7]. The ingestion of dyes by human 36 beings may cause cancer, mutagens, teratogens, cardiovascular shock, vomiting, 37 gastrointestinal pain, diarrhoea, etc., and contamination of water with dyes causes serious 38 problems for the environment and aquatic life [8–11]. Numerous studies have used many 39 methods to remove dyes such as degradation, coagulation, photocatalysis, flocculation, 40 41 hydrogen peroxide, adsorption, oxidation, irradiation, ion exchange, reverse osmosis, advanced oxidation, membrane filtration, precipitation, etc. [12–15]. Adsorption is a good technique 42 because of its ease of operation, efficacy, high efficiency, and low energy demand. There are 43 many adsorbents available and they are effective in regeneration and can be reused [16–23]. 44

45 Agricultural solid wastes are lignocellulosic materials and their main components are 46 cellulose, lignin, and hemicelluloses, lipids, proteins, etc. [16]. Agricultural wastes include organic products, vegetables, fruits, meat, poultry, dairy items, and harvests. Agricultural solid wastes are extensively used to eliminate dyes from environmental wastewaters [24–27]. These materials are renewable and abundant in large quantities and have high potential as sorbents owing to the variety of functional groups (–OH, –C=O, –C–O, –NH₂) on their surface [28]. As a result, agricultural wastes can be used as an economic and eco-friendly adsorbent [29]. The date stone as agricultural solid waste used for dyes removal has been studied by others, but its performance as an adsorbent was limited because of its undeveloped porous structure [30–32].

54 Synthesizing approach and reaction parameters can have a significant influence on 55 nanomaterial's magnetic, photocatalytic, and electrical properties [33, 34]. Nanostructures of 56 CuFe₂O₄ have been developed by such reactions as solid-state [35, 36], sonochemical [37, 38], 57 and hydrothermal [39, 40]. Besides, the ultrasonic-assisted approach is regarded as a simple, 58 rapid, cost-effective, and eco-friendly method for creating nanostructured materials such as 59 metals, metal chalcogenides, bimetal oxide, and graphene [41, 42].

In this work, DS@CuFe₂O₄ nanocomposite synthesized from date stones powder and 60 CuFe₂O₄ nanoparticles were used for the removal of rhodamine and methyl orange from the 61 aqueous solution. The synthesized nanocomposite was characterized by different analytical 62 instruments such as Brunauer Emmett Teller (BET), Fourier transform infrared (FTIR), 63 scanning electron microscope (SEM), and transition electron microscope (TEM) analysis. The 64 research team investigated the influence of different experimental conditions through altering 65 operational parameters such as initial pH of the solution, adsorbent dosage, contact time, 66 pollutant concentration, and temperature. The RhB and MO adsorption on DS@CuFe₂O₄ were 67 evaluated by kinetics (pseudo-first-order and pseudo-second-order) and equilibrium (Langmuir, 68 Freundlich, and Temkin) models and thermodynamics parameters. The reusability of 69 DS@CuFe₂O₄ nanocomposite was also investigated. 70

71 **2. Experimental**

72 **2.1.** Chemicals and reagents

Chemicals and reagents used in this study were as follows: Copper chloride dehydrate
(CuCl₂, 2 H₂O), ferric chloride solution (FeCl₃, 4H₂O), rhodamine B (cationic dye,
C₂₈H₃₁N₂O₃Cl, CI=45170, MW=479.01 g mol⁻¹), methyl orange (anionic dye, C₁₄H₁₄N₃NaO₃S,
CI=13025, MW=327.33 g mol⁻¹), deionized water, HCl, and NaOH. All chemicals were of
analytical grade and purchased from Sigma-Aldrich.

78 2.2. Synthesis of CuFe₂O₄ nanoparticles

Copper chloride dihydrate (CuCl₂, 2 H₂O) was used as a precursor and was dissolved 79 in deionized water, and then it was mixed drop by drop with ferric chloride solution 80 (FeCl₃.4H₂O). Then, ultrasonic radiation with high intensity (100 W cm⁻²), operating at 50 kHz, 81 was used under ambient air for 1 h. The titanium horn was embedded to a depth of 4 cm in the 82 solution. The reaction cell was not thermostated and the final temperature was 50 °C. After 83 sonication, the solution was centrifuged at 5000 rpm for 4 min and rinsed with deionized water. 84 Finally, one portion of the sample was over-dried (80 °C) for 12 h. The second portion of the 85 sample was prepared by calcination in the furnace at 600 °C for 4 h. 86

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2.3. Synthesis of DS@CuFe₂O₄ nanocomposite

Date stones (DS) were collected in Tinghir (South-East Morocco). The material was, crushed, sieved, and washed with ethanol and deionized water, then dried at 105 °C overnight. The DS@CuFe₂O₄ (date stones modified by CuFe₂O₄) nanocomposite was synthesized by addition of 1 g of date stones powder prepared and 2 g of CuFe₂O₄ nanoparticles in deionized water (1:2 v/v). The mixture was stirred for 3 h at room temperature. Then it was centrifuged, filtered, and dried in an oven for 16 h at 80 °C. After, the annealing process was conducted in a tube muffle furnace at 800 °C for 2 h to obtain the date stones nanoparticles (DS@CuFe₂O₄).

95 **2.4. Characterization of adsorbent**

The prepared adsorbent is characterized by various techniques. Brunauer Emmett Teller 96 (BET) model using Belsorp Mini II and Barrett-Joyner-Halenda (BJH) methods were employed 97 to evaluate the specific surface area and total pore volume, and diameter pore of 98 DS@CuFe₂O₄ Fourier transform infrared (FTIR) spectroscopy with resolution 4 cm⁻¹ in a 99 spectrometer Jasco 4100 and coupled with attenuated total reflectance (ATR) technique in the 100 range 4000-400 cm⁻¹ was used to determine the functional groups present in surface adsorbent. 101 Scanning electron microscope (SEM) on JEOL, JSM-IT200 at tension 20 kV and transition 102 electron microscope (TEM) using Philips CM-30 were used to specify the morphology of 103 104 DS@CuFe₂O₄.

105 2.5. Removal of RhB and MO using DS@CuFe₂O₄

The RhB and MO sorption were conducted in 250 mL Erlenmeyer flasks on a 106 107 thermostatic shaker in batch mode. A quantity of DS@CuFe₂O₄ was added to 50 mL of RhB or MO dye solution (100 mg L⁻¹). The mixture was agitated at 170 rpm at 26 ± 1 °C for 50 min. 108 The influence of different parameters such as solution pH (3–11), DS@CuFe₂O₄ dosage (0.2– 109 1.2 g L^{-1}), contact time (0–120 min), initial dye concentration (50–400 mg L^{-1}), and 110 temperature (10–50 °C) on dyes adsorption was evaluated. The pH of the solution was adjusted 111 by 0.1 M HCl or 0.1 M sodium NaOH. The point of zero charge (PZC) value of DS@CuFe₂O₄ 112 was determined using the method reported by Fiol and Villaescusa [43]. After completing the 113 experiment, the dye solution was filtered through centrifuging at 3500 rpm for 5 min. The 114 concentrations of residual RhB and MO were measured using a UV/Vis spectrophotometer 115 (2300/Techcomp) at 557 and 465 nm as λ_{max} of RhB and MO, respectively. The quantity 116 adsorbed $q_e (mg g^{-1})$ and removal efficiency (%) of RhB or MO onto DS@CuFe₂O₄ were 117 calculated by the equations given below: 118

119
$$q_e = \frac{(C_0 - C_e) \times V}{W} \tag{1}$$

120 % Removal =
$$\frac{(C_0 - C_e)}{C_0} \times 100$$
 (2)

121 Where, $C_0 \text{ (mg } \text{L}^{-1})$ and $C_e \text{ (mg } \text{L}^{-1})$ are the RhB or MO concentrations before and after 122 adsorption, respectively, V (L) is the dye solution volume and W (g) is the weight of 123 DS@CuFe₂O₄ used.

124 **3. Results and discussion**

125 **3.1. DS@CuFe2O4 characterization**

126 **3.1.1. BET and FTIR analysis**

Using the Brunauer Emmett Teller (BET) and Barrett-Joyner-Halenda (BJH) methods (Figure1a), the obtained average surface area was $52.16 \text{ m}^2 \text{ g}^{-1}$, and the average pore diameter was 17.34 nm and the total pore volume was $0.086 \text{ cm}^3 \text{ g}^{-1}$.

130 Infrared spectroscopy helps us to a better comprehension of the functional group, phase purity, and structural bonding between the metal and oxides in the nanocomposite. The 131 spectra FTIR of DS and DS@CuFe₂O₄ are shown in Figure1b. On the spectrum of DS, the 132 bond at 3435 cm⁻¹ corresponds to hydroxyl -OH stretching vibration found on cellulose 133 hemicelluloses and lignin [44, 45]. The peak observed at 1747 cm⁻¹ is attributed to stretching 134 vibration of -C=O owing to carboxyl group -COOH and may be assigned to carboxylic acids 135 of xylan in hemicelluloses [20, 46]. The peak at 1147 cm⁻¹ is attributed to -C-O stretching 136 vibration of carboxylic acids and alcohols [47-49]. After modification of the DS with CuFe₂O₄ 137 nanoparticles, we note the presence of the peaks at 586 cm^{-1} and 475 cm^{-1} corresponds to the 138 Fe and Cu [50-52], respectively. These peaks confirmed the complexation of CuFe₂O₄ 139 nanoparticles with DS. 140

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To determine the quality of microstructures, the CuFe₂O₄ and DS@CuFe₂O₄ were examined by scanning electron microscope (SEM) and transition electron microscope (TEM). According to **Figure 2a**, **b**, the DS surface has different micropores in various shapes and sizes. **Figure 2c**, **d** shows CuFe₂O₄ surface and **Figure 2e**, **f** shows the development of DS surface micropores and also the dispersion of CuFe₂O₄ nanoparticles over it after modification.





- **Figure2**. SEM images of DS (\mathbf{a},\mathbf{b}) , CuFe₂O₄ (\mathbf{c}) , DS@CuFe₂O₄ (\mathbf{d}) ,
- 153

TEM images of CuFe₂O₄ (\mathbf{e}), and DS@CuFe₂O₄ (\mathbf{f}).

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155 3.2. RhB and MO adsorption on DS@CuFe₂O₄

156 **3.2.1. Effect of pH**

To investigate the effect of initial solution pH on adsorption of RhB and MO in water, the batch experiments were conducted at different pH ranging from 3 to 11 (**Figure 3a**) at an initial concentration of 100 mg L⁻¹ of dye, 0.2 g L⁻¹ of adsorbent dosage and 120 min of contact time. The point of zero charge (PZC) is a crucial parameter to understand the adsorption process. As **Figure 3b** shows, pH_{PZC} of DS@CuFe₂O₄ was 4.8. The highest removal efficiency was 84.65 % for RhB at pH=8 and 80.85 % for RhB at pH=5. As a result, the DS@CuFe₂O₄ surface charge will be positively charged at pH<pH_{PZC} (adsorption of anionic 164 dye MO was favourable) and negatively charged when pH>pH_{PZC} (adsorption of cationic dye
165 RhB was favourable) [53, 54].





Figure3. Effect of pH on RhB and MO adsorption (**a**) and pH_{PZC} of DS@CuFe₂O₄ (**b**).



3.2.2. Effect of DS@CuFe2O4 dosage

To evaluate the effect of DS@CuFe₂O₄ nanocomposite dosage, the adsorption 168 experiments were carried out with different dosages of 0.2 to 1.2 g L^{-1} whereas other 169 parameters were kept constant (RhB or MO concentration=100 mg L^{-1} , contact time =120 170 171 min, pH (RhB)=8, and pH (MO)=5). Figure 4a shows the results obtained. The RhB removal increased from 64.66 to 97.84 % by increasing the adsorbent dosage from 0.2 to 0.4 g L^{-1} , and 172 the MO removal increased from 47.46 to 86.81 % by and from 0.2 to 0.6 g L^{-1} . Results imply 173 that the number of active adsorption sites for RhB and MO adsorption is corresponding to the 174 applied dose, which prompts higher removal efficiency [55]. After equilibrium between 175 the adsorbent and dye in the solution, the removal percentage remains consistent at higher 176 dosages (> 0.4 g L^{-1} for RhB and > 0.6 g L^{-1} for MO). The optimum adsorbent dosage was 177 considered 0.4 g L^{-1} RhB and 0.6 g L^{-1} to reach maximum RhB and MO removal efficiency, 178 respectively. 179

180 **3.2.3. Effect of contact time**

The contact time effect on adsorption of RhB and MO onto DS@CuFe2O4 was examined 181 at an initial concentration of 100 mg L^{-1} of dye and 0.4 g L^{-1} and 0.6 g L^{-1} of adsorbent dosage 182 for RhB and MO, respectively. As can be seen from Figure 4b, the RhB and MO adsorption 183 was fast at first, but they declined after that. This may be attributed to many sites that are 184 accessible on the surface of the nanocomposite in the initial stage [56]. With decreasing in 185 several active sites, the adsorption rate became consistent [57]. Experimental data showed 186 that equilibrium was achieved in 50 min with 244.40 mg g^{-1} and 159.72 mg g^{-1} adsorption 187 capacity of RhB and MO, respectively. 188

189

3.2.4. Effect of initial dye concentration

As a function of initial RhB and MO concentrations, two factors of removal efficiency 190 and equilibrium adsorption capacities were investigated. The initial RhB and MO 191 concentrations varied from 50 to 400 mg L^{-1} with keeping all other parameters consistent 192 (DS@CuFe₂O₄ dosage: 0.4 g L⁻¹ (RhB): 0.6 g L⁻¹ (MO), temperature: 26 ± 1 °C, contact time: 193 50 min, pH (RhB) = 8, and pH (MO) = 5. The results are depicted in Figure 4c. As illustrated 194 in Figure 4c, by increasing RhB and MO concentrations, adsorption capacity progressively 195 increased owing to the occupation of all available sites on the surface of nanocomposite by RhB 196 197 and MO molecules. But, a plateau was not achieved in the adsorption capacity, suggesting active sites are still available and no saturation occurred [58]. On the other hand, removal 198 efficiency decreased because of increasing the competition among RhB and MO molecules for 199 occupying available sites. Dye initial concentration is an important factor in the adsorption 200 process because as a driving force, it overcomes the resistance of mass transfer between solution 201 202 and solid phases [59].



204 205

Figure 4. Percentage of RhB and MO removal as a function DS@CuFe₂O₄ dosage (a), Effects of contact time (b), initial dye concentration (c), and temperature (d) on RhB

207 208

206

and MO adsorption using DS@CuFe₂O₄.

3.2.5. Effect of temperature 209

Figure 4d shows the RhB and MO adsorption on DS@CuFe₂O₄ using 50 mL of 100 210 mg L^{-1} dye solution at different temperatures (10, 20, 30, 40, and 50 °C). It was seen that 211 temperature was increased from 10 to 50 °C for adsorption capacity of dye increased from 212

213 228.86 to 246.84 mg g⁻¹ for RhB and from 105.30 to 157.51 mg g⁻¹ for MO at 50 min of contact 214 time and pH=8 for RhB and pH=5 for MO. This increase was because the mobility accelerated 215 of dye molecules with increasing of temperature and therefore the sites at the surface of 216 adsorbent were active, and the adsorption is an endothermic reaction [59].

217 **3.3. Adsorption modeling**

218 **3.3.1. Kinetic examination**

The RhB and MO adsorption on DS@CuFe₂O₄ was evaluated using two kinetic (pseudofirst-order and pseudo-second-order) models and are expressed by the equations below [60– 62]:

222
$$Log(q_e - q_t) = Log(q_e) - \frac{K_1}{2.303}t$$
 (3)

223
$$\frac{t}{q_t} = \frac{1}{K_2 q_e^2} + \frac{1}{q_e} t$$
(4)

Where, q_t (mg g⁻¹) and q_e (mg g⁻¹) are the amounts adsorbed at t and equilibrium, 224 respectively, t is the time of reaction, K_1 (min⁻¹) and K_2 (g mg⁻¹ min⁻¹) are the constants related 225 to the first-order and second-order, respectively. Figure 5 shows the kinetic adsorption curves 226 plotted for the two kinetic models. Table 1 shows the parameters for linear fitting. The 227 experimental data observed fit with the second-order model. It can be found that the correlation 228 coefficients r^2 are very near to 1 for the two dyes. The experimental $q_{e,exp}$ values are also closer 229 to the theoretically calculated $q_{e, cal}$ values for the second-order model. These results 230 demonstrated that RhB and MO adsorption on DS@CuFe2O4 follows a second-order kinetic 231 232 model.

The optimization procedure requires an error function for evaluating the fit of the equation to the experimental data. The residual root means square error (*RMSE*) and the sum of squares error (*SSE*) is calculated from the following Eqs. (5) and (6), respectively [63, 64]:

236
$$RMSE = \sqrt{\sum_{i=1}^{N} \frac{(q_{e,exp} - q_{e,cal})^2 i}{N}}$$
(5)

237
$$SSE = \sum_{i=1}^{N} (q_{e,exp} - q_{e,cal})^2 i$$
(6)

N= Number of experimental points.



Figure 5. Kinetic curves of RhB and MO adsorption on DS@CuFe₂O₄: pseudo-first-order (**a**) and pseudo-second-order (**b**) models.

Table 1. Kinetic model parameters for RhB and MO adsorption on DS@CuFe₂O₄.

Model	Parameter	RhB	MO
	$q_{e,,exp} (\mathrm{mg} \mathrm{g}^{-1})$	245.79	162.81
Pseudo-first-order	K_1 (min ⁻¹)	0.069	0.047
	$q_{e, cal} (\mathrm{mg}\;\mathrm{g}^{-1})$	91.28	63.40
	r^2	0.912	0.820
	RMSE	1.016	2.326
	SEE	4.347	3.192
	K_2 (g mg $^{-1}$ min $^{-1}$)	0.001	0.002
Pseudo-second-order	$q_{e, cal} (\mathrm{mg}\;\mathrm{g}^{-1})$	256.41	169.49
	r^2	0.997	0.999
	RMSE	0.945	2.072
	SEE	3.026	2.438

246 **3.3.2.** Equilibrium investigation

The correlation between adsorption capacity and dye concentration in a liquid phase at equilibrium was determined using Langmuir, Freundlich, and Temkin isotherm models and is represented by the equations below, respectively [65–67]:

250
$$\frac{C_e}{q_e} = \frac{1}{Q_m K_L} + \frac{C_e}{Q_m}$$
(7)

$$Lnq_e = LnK_F + \frac{LnC_e}{n}$$
(8)

$$q_e = BLnK_T + BLnC_e \tag{9}$$

Where, Q_m (mg g⁻¹) is the maximum dye per gram of adsorbent, K_L (L mg⁻¹) is the 253 constant of Langmuir isotherm, K_F ((mg g⁻¹)(L mg⁻¹)^{1/n}) is the constant related to Freundlich 254 isotherm, K_T (L g⁻¹) is the constant of Temkin isotherm and B is the constant related to the 255 heat adsorption. The results obtained are shown in Figure 6 and the calculated parameters are 256 given in **Table 2**. Based on correlation coefficient r^2 , the Langmuir model best described the 257 258 RhB and MO adsorption equilibrium data. Langmuir model suggests the dye adsorption occurs as a monolayer from the homogeneous surface of the adsorbent [68]. A similar observation was 259 found in other studies, which also have shown the successful prediction of adsorption isotherm 260 data using Langmuir isotherm as compared to Freundlich and Temkin isotherm models [69-261 72]. 262



Model	Parameter	RhB	MO
	$Q_m (\mathrm{mg}\;\mathrm{g}^{-1})$	555.56	303.03
Langmuir	K_L (L mg ⁻¹)	0.097	0.057
	r^2	0.995	0.993
	$K_F ((\text{mg g}^{-1}) (\text{L mg}^{-1})^{1/n})$	137.414	84.040
Freundlich	Ν	3.617	4.385
	r^2	0.748	0.922
	$K_T (\mathrm{L} \mathrm{g}^{-1})$	3.246	6.472
Temkin	В	84.503	37.670
	r^2	0.883	0.938

Table 2. Isotherm model parameters for RhB and MO adsorption on DS@CuFe₂O₄.

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274 **3.3.3. Thermodynamic analysis**

The thermodynamic parameters of RhB and MO adsorption on DS@CuFe₂O₄ such as the free energy ΔG° , the enthalpy ΔH° , and the s entropy ΔS° were calculated by the equations below [73, 74]:

$$\Delta G^{\circ} = -RTLnK_C \tag{10}$$

279
$$LnK_C = \frac{\Delta S^{\circ}}{R} - \frac{\Delta H^{\circ}}{RT}$$
(11)

Where, R (8.314 J mol⁻¹ K⁻¹) is the constant of perfect gases, T (K) is the absolute 280 temperature and K_C is the equilibrium constant, ΔH° was obtained from the slope of LnK_C 281 versus 1/T (K⁻¹) and ΔS° was obtained from y-intercept for adsorption of dye. Table 3 shows 282 the thermodynamic adsorption parameters of RhB and MO on DS@CuFe₂O₄. The negative 283 value of ΔG° at five temperatures suggested the feasibility and spontaneity of the RhB and MO 284 adsorption on DS@CuFe₂O₄. This adsorption is physical because the ΔG° was lower than 0 kJ 285 mol⁻¹ [75]. The positive ΔH° values verified the endothermic nature of the adsorption process 286 [46, 76]. The positive ΔS° values indicate that the disorder increases at the adsorbent/solution 287 interface [77, 78]. 288

289

290

Dye	<i>T</i> (K)	ΔG° (kJ mol ⁻¹)	$\Delta H^{\circ} (\text{kJ mol}^{-1})$	$\Delta S^{\circ} (\mathbf{J} \operatorname{mol}^{-1} \mathbf{K}^{-1})$
	283	-06.394		
	293	-07.804		153.044
RhB	303	-09.615	37.713	
	313	-10.327		
	323	-11.702		
	283	-01.315		
	293	-03.412	40.931	149.610
MO	303	-04.106		
	313	-05.203		
	323	-06.929		

Table 3. Thermodynamic parameters for RhB and MO adsorption on DS@CuFe₂O₄.

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292

294 **3.4.** Comparison with other adsorbents

The maximum adsorption capacity of DS@CuFe₂O₄ for RhB and MO was compared with the previous study; see **Table 4**. The results show that DS@CuFe₂O₄ has good adsorption performance on the RhB and MO removal, better than some adsorbents previously reported in the literature.

299

Table 4. Comparison of adsorption capacity of RhB and MO with previous studies.

Adsorbent	Q _m (mg	Q _m (mg g ⁻¹)	
	RhB	MO	
Magnetic pectin/ Chlorella vulgaris	_	109.11	[79]
Ghum ghati/Fe ₃ O ₄	529.10	_	[69]
α -MnO ₂ nanoparticles	_	116.10	[72]
Magnetic activated carbon/CeO ₂	324.60	_	[80]
ZnO/Zr-MOF(bpy)	918.90	_	[81]
Graphene boron nitride/SiO ₂	625.00	_	[70]
Fe ₃ O ₄ /C	87.32	38.03	[82]
Graphene oxide/carbon nanotube	248.48	66.96	[83]
Bentonite/ carbon nanotube	148.20	_	[71]
PANi-BiVO ₄	—	75.90	[84]
Biobased magnetic hollow particles	50.40	_	[85]
Functionalized-CNTs loaded TiO ₂	42.85	_	[86]
DS@CuFe ₂ O ₄	555.56	303.03	This study

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301

302

304 3.5. Reusability of DS@CuFe2O4

After adsorption of dye, the DS@CuFe₂O₄ was regenerated by washing many times with 0.01 M HCl and 0.01M NaOH for their reusability in the RhB and MO removal from aqueous solution, respectively; see the results in **Figure7**. It is noted that adsorption efficiency decreases from 98.54 to 83.15 % for RhB and from 95.22 to 79.08 % for MO after six cycles. This decrease was attributed to the occupation of available sites on the DS@CuFe₂O₄ surface [87]. The above result further indicated the DS@CuFe₂O₄ could be reused for the removal of organic dyes in wastewater.



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313

Figure 7. Reusability of DS@CuFe₂O₄ in the removal of RhB and MO dyes.

4. Conclusion

In this study, a novel nanocomposite was synthesized with date stones modified by $CuFe_2O_4$ and it was applied for rhodamine B and methyl orange removal from aqueous solutions. The results of the adsorption experiment conducted in batch mode revealed optimum conditions for RhB and MO adsorption by $DS@CuFe_2O_4$ nanocomposite. Dye removal was maximum at pH=8 for RhB and pH=5 for and RhB and equilibrium were achieved

in 50 min. The result of FTIR, SEM, and TEM characterization verified the dispersion and complexation of $CuFe_2O_4$ nanoparticles with DS. Kinetic and isotherm models were fitted to the experimental data, showing that pseudo-second-order kinetic and Langmuir isotherm models were best fitted to the data. The maximum adsorption capacity was 555.56 and 303.03 mg g⁻¹ for RhB and MO, respectively. The thermodynamic study revealed that physisorption is the dominant mechanism and adsorption of RhB and MO to nanocomposite is endothermic. The finding suggested that DS@CuFe_2O_4 nanocomposite could be considered as an efficient adsorbent to remove dyes from aqueous solutions.

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317 **Disclosure Statement**

318 No potential conflict of interest was reported by the authors.

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